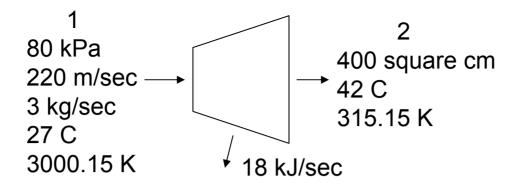
Problem Set 1 (PS1) Due Tuesday January 24

- 1. Air at 80 kPa, 27 C and 220 m/sec enters a diffuser at a rate of 3 kg/sec and leaves at 42 C. The exit area of the diffuser is 400 square cm. The air looses heat a a rate of 18 kJ/sec. Determine the exit velocity and the exit air pressure
- 2. In an insulated heat exchanger air is heated at atmospheric pressure from 25 C to 100 C and 2 kg/sec of water is cooled at atmospheric pressure from 150 C to 100 C. What is the entropy change for the air stream, the water stream and for the overall heat transfer process?
- 3. 3 lbs of air is expanded in an adiabatic isentropic process from 500 R and a gage pressure 200 psi to a gage pressure off 100 psi. Atmospheric pressure is 14.6 psi. What are the temperature, pressure, specific density and total volume at the end of the process?



steady flow energy equation

steady flow energy equation
$$m\left(c_p T_1 + \frac{u_1^2}{2 \times 1000}\right) + Q = m\left(c_p T_2 + \frac{u_2^2}{2 \times 1000}\right)$$

$$3 \text{ kg}\left(1.005 \times 300.15 \frac{220^2}{2000}\right) + 18 \text{ kJ/sec} = 3 \text{kg}\left(1.005 \times 315.15 \frac{u_2^2}{2000}\right)$$

$$941 + 18 = 950.18 + .0015 u_2^2$$

$$u_2 = 76.7 \text{ m/sec}$$
continuity equation
$$m = \rho_2 A_2 u_2$$

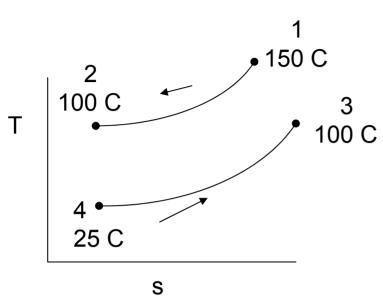
$$m = \rho_2 A_2 u_2$$

ideal gas law

$$\mathbf{m} = \frac{\mathbf{p}_2}{\mathbf{R} \, \mathbf{T}_2} \mathbf{A}_2 \, \mathbf{u}_2$$

$$p_2 = \frac{\text{m R T}_2}{\text{A}_2 \text{u}_2} = \frac{3 \times 8.324 \text{ kPa/kgmole K} \times 315.5 \text{ K}}{28.97 \times .04 \text{ m}^2 \times 76.68 \text{ m/sec}} = 88.46 \text{ kPa}$$

PS1.2



energy balance

$$Q_{\text{water}} = Q_{\text{air}}$$

$$m_{\text{water}} \times c_p \times (T_1 - T_2) = m_{\text{air}} \times c_p \times (T_1 - T_2)$$

$$m_{air} = \frac{2 \text{ kg} \times 4.18 \text{ kJ/kg K} \times (150-100)}{1.005 \text{ kJ/kg K} \times (100-25)}$$

$$m_{air} = 5.5 kg/sec$$

entropy change

$$\Delta S_{air} = m_{air} c_p ln \left(\frac{T_2}{T_1}\right) - R ln \left(\frac{p_2}{p_1}\right)$$

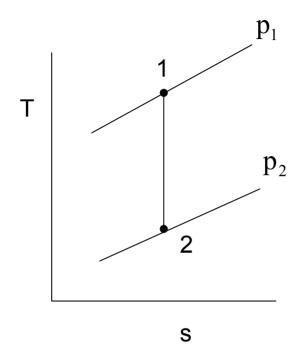
$$\Delta S_{air} = 5.5 \times 1.005 \times ln \left(\frac{373.15}{298.15} \right) = +1.228 \text{ kJ/K}$$

$$\Delta S_{\text{water}} = 2 \times 4.18 \times \ln \left(\frac{373.15}{423.15} \right) = -1.0512 \text{ kJ/K}$$

$$\Delta S_{\text{process}} = \Delta S_{\text{air}} + \Delta S_{\text{water}} = +1.228 - 1.0512$$

$$\Delta S_{\text{process}} = +.177 \text{ kJ/K}$$

$$\Delta S_{\substack{\text{isolated} \\ \text{system}}} \ge 0$$



ideal gas law

$$\rho_1 = \frac{p}{RT} = \frac{214.6 \text{ lbf/in}^2 \times 144 \text{ in}^2/\text{ft}^2}{\frac{1545.15 \text{ ft lbf/lbmole}}{28.97} \times 500 \text{ R}}$$

$$\rho_1 = 1.158 \, \text{lbm/ft}^3$$

isentropic process

$$\frac{T_2}{T_1} = \left(\frac{p_2}{p_1}\right)^{\frac{\gamma - 1}{\gamma}} = \left(\frac{114.6}{214.6}\right)^{.2857} = .8359$$

$$T_2 = 500 \times .8359 = 417.96 R$$

$$\frac{\rho_2}{\rho_1} = \left(\frac{p_2}{p_1}\right)^{\frac{1}{\gamma}} = \left(\frac{114.6}{214.6}\right)^{.7143} = .6388$$

$$\rho_2 = .6388 \times 1.158 = .7398 \text{ lbm/ft}^3$$

$$V_2 = \frac{m}{\rho} = \frac{3 \text{ lbm}}{.7398} = 4.055 \text{ ft}^3$$